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# Electrochemical properties of cobalt hydroxychloride microspheres as a new anode material for Li-ion batteries

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The use of cobalt hydroxychloride [ $\text{Co}_2(\text{OH})_3\text{Cl}$ ] as an anode material for lithium ion batteries (LIBs) is investigated using spherical shape and ultrafine nanocrystals directly formed by spray pyrolysis from spray solution of cobalt chloride salt. Dot-mapping images of the resulting powders reveal a uniform distribution of Co, O, and Cl throughout the powder. The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder prepared directly by spray pyrolysis exhibits a high thermal stability at temperatures below  $220^\circ\text{C}$ , as well as having superior electrochemical properties compared with those of the  $\text{CoCl}_2(\text{H}_2\text{O})_2$  and  $\text{CoO}$  powders prepared by the same process. The initial discharge capacities of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  and  $\text{CoO}$  powders at a constant current density of  $1000\text{ mA g}^{-1}$  are found to be 1570 and  $1142\text{ mA h g}^{-1}$ , respectively, and their initial Coulombic efficiencies are 72 and 70%. The discharge capacities of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  and  $\text{CoO}$  powders after 100 cycles are 955 and  $632\text{ mA h g}^{-1}$ , respectively. The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders have a high discharge capacity of  $609\text{ mA h g}^{-1}$  even after 1000 cycles at a high current density of  $5000\text{ mA g}^{-1}$ .

The high energy density of lithium ion batteries (LIBs) makes them suitable for various applications, ranging in size from portable electronic devices to zero-emission vehicles, but existing LIB technology is rapidly reaching its limits in terms of energy density (per volume) and specific energy (per weight)<sup>1–3</sup>. At present, graphitic materials are widely used as the anode material in lithium-ion batteries, mostly due to their low price and high reversibility. However, graphitic anodes inherently exhibit a relatively low capacity value (theoretical value equal to  $372\text{ mA h g}^{-1}$ ), and are thus inadequate for high power applications<sup>4–7</sup>. In order to ensure the successful use of Li-ion batteries in a wider variety of applications, for example electric cars, it is imperative to overcome at least some of the challenges related to obtaining a higher energy density, longer cycle life, improved high rate capability and greater safety<sup>8–13</sup>. A great deal of attention has therefore been focused on the anode materials used, as there is significant potential in this area for greatly improving battery performance<sup>2,14–19</sup>; the use of a more suitable anode material being by far the most effective means of achieving a high performance. To this end, metal oxides, sulfides, nitrides, fluorides, and oxysulfides have all been extensively explored as potential anode materials for lithium ion batteries<sup>20–29</sup>; their attraction being their ability to store excess lithium ions by a conversion reaction that results in a significantly larger reversible capacity than graphite.

Recently, copper hydroxychloride [ $\text{Cu}_2\text{Cl}(\text{OH})_3$ ] was studied as a promising anode material for LIBs<sup>30</sup>, this material being able to reversibly store and release Li ions via a conversion reaction that is widely observed in  $\text{CuO}$  and  $\text{CuS}$  electrodes. The discharge capacities of chemically synthesized  $\text{Cu}_2\text{Cl}(\text{OH})_3$  powders at a low current density of  $100\text{ mA g}^{-1}$  were found to be 1100 and  $430\text{ mA h g}^{-1}$  for the 1<sup>st</sup> and 20<sup>th</sup> cycles, respectively. Moreover, although copper based materials containing  $\text{CuO}$  and  $\text{CuS}$  have poor electrochemical properties compared with the other transition metal-based materials such as Co, Mn, and Fe; metal hydroxychlorides excluding copper have not been studied as potential electrode materials for LIBs to the best of the authors' knowledge<sup>20–23,31–33</sup>.

Cobalt basic salts, expressed using a general formula of  $\text{Co}(\text{OH})_{2-x}(\text{A}^{n-})_x$  ( $\text{A}^-$ :  $\text{Cl}^-$ ,  $\text{NO}_3^-$ ,  $\text{SO}_4^{2-}$ ,  $\text{CO}_3^{2-}$ , etc.), have been extensively studied over the last two decades because of the important electric, magnetic, and catalytic properties of the metal oxides formed upon their thermal decomposition<sup>34–37</sup>. However, the preparation process to obtain cobalt basic salts with controlled morphologies, and their resulting electrochemical properties, have not been reported. In this study, cobalt hydroxychloride [ $\text{Co}_2(\text{OH})_3\text{Cl}$ ] is therefore studied for the first time as a potential anode material for LIBs. The spherical shape of  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders produced by a simple one-pot spray pyrolysis process is found to result in superior electrochemical properties. Furthermore, the discharge capacity of bare  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders, i.e., without carbonaceous materials generally improve the electrical



conductivity as well as acting as buffer layer for large volume changes during cycling, was high as  $609 \text{ mA h g}^{-1}$  after 1000 cycles at a high current density of  $5000 \text{ mA g}^{-1}$ .

## Results

The crystal structures of the powders were found to be strongly affected by their respective preparation temperatures, as shown in Figure 1. Those powders prepared at temperatures of 500 and  $900^\circ\text{C}$  had primary crystal structures of  $\text{CoCl}_2(\text{H}_2\text{O})_2$  and  $\text{CoO}$ , respectively; however, the XRD pattern of the powders prepared directly by spray pyrolysis at  $700^\circ\text{C}$  indicated main peaks of  $\text{Co}_2(\text{OH})_3\text{Cl}$  crystals, and minor peaks of  $\text{CoCl}_2(\text{H}_2\text{O})_2$  and  $\text{CoO}$  crystals. Decomposition of  $\text{Co}_2(\text{OH})_3\text{Cl}$  into  $\text{CoO}$  was found to occur at a high preparation temperature of  $900^\circ\text{C}$  under a nitrogen atmosphere; and consequently, the optimum direct preparation temperature for  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders by spray pyrolysis is located somewhere between 500 and  $900^\circ\text{C}$ .

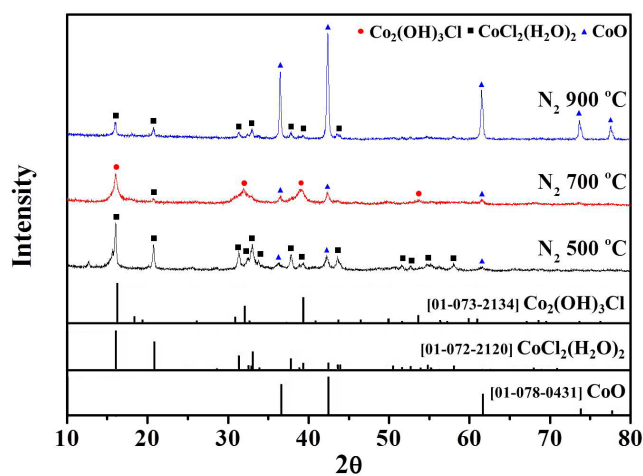
The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders prepared directly by spray pyrolysis at  $700^\circ\text{C}$  were found to have a spherical shape and porous structure, as shown by the SEM and TEM images in Figures 2a–2d. Moreover, the high resolution TEM image in Figure 2e shows the presence of ultrafine nanocrystals of less than 10 nm in size, with clear lattice fringes separated by 0.59 and 0.42 nm. The dot-mapping images of the powders, as shown in Figure 2f, reveal a uniform distribution of Co, O, and Cl throughout the powder. The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder exhibiting both a spherical shape and ultrafine nanocrystals was directly formed from a single droplet of cobalt chloride salt by means of drying and decomposition.

Figures 3a and 3b show the EDX spectrum and thermogravimetric (TG) curve, respectively, for  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders prepared directly by spray pyrolysis at  $700^\circ\text{C}$ . The respective concentrations of Co, O, and Cl were determined from the EDX spectrum as 45.4, 29.1, and 25.5 atomic%; and the mole ratio of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  and  $\text{CoCl}_2(\text{H}_2\text{O})_2$  phases was estimated at 0.92 : 0.08 when the  $\text{CoO}$  content of the powders was ignored. The TG curve for the powders measured under air atmosphere exhibited three distinct weight losses below  $1200^\circ\text{C}$ ; the reaction occurring with each decrease in weight being described in Figure 3b and summarized as follows: The first weight loss occurs below  $380^\circ\text{C}$ , and is due to the oxidation of  $\text{Co}_2(\text{OH})_3\text{Cl}$  to form  $\text{CoCl}_2$ ,  $\text{CoO}_3$ , and  $\text{H}_2\text{O}^{34}$ ; the second weight loss occurs between 400 and  $600^\circ\text{C}$ , due to the decomposition of  $\text{CoCl}_2$  into  $\text{Co}_3\text{O}_4^{38}$ ; and the final weight loss occurs above  $1100^\circ\text{C}$ , due to the reduction of  $\text{Co}_3\text{O}_4$  into  $\text{CoO}^{39}$ . Despite this, the cobalt hydroxylchloride prepared directly by spray pyrolysis had high thermal stability at temperatures below  $220^\circ\text{C}$ . Figure S1a shows the  $\text{N}_2$  adsorption and desorption isotherms of the powders prepared by

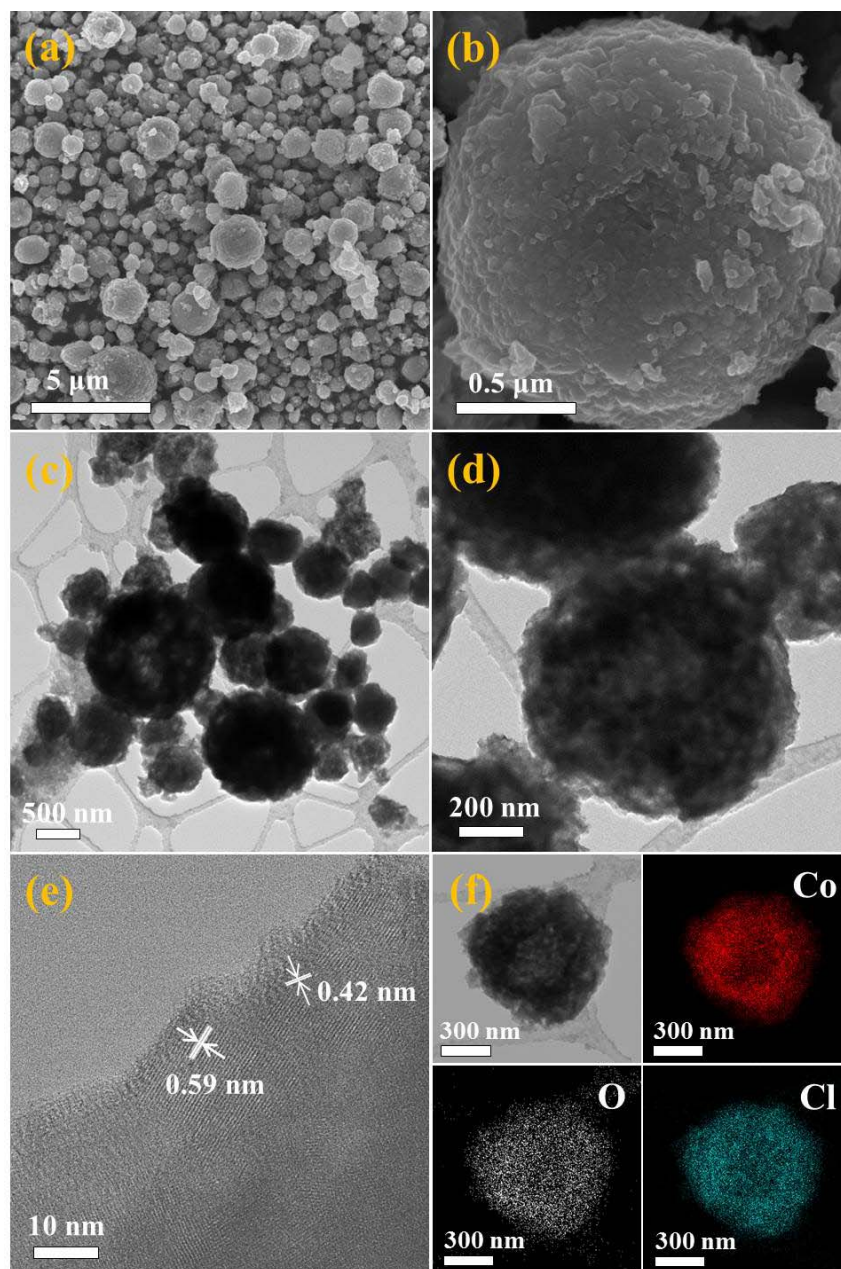
spray pyrolysis of a solution containing cobalt chloride at various temperatures, in which the hysteresis loops resemble the type-H3 IUPAC (International Union of Pure and Applied Chemistry) isotherm classification. The pore size distributions, as shown in Figure S1b, indicate that the powders have a mesoporous structure irrespective of their preparation temperature. The BET surface areas of the powders prepared at 500, 700, and  $900^\circ\text{C}$  were subsequently determined as 13, 6, and  $4 \text{ m}^2 \text{ g}^{-1}$ , respectively.

The electrochemical properties of those powders with primary crystal structures of  $\text{CoCl}_2(\text{H}_2\text{O})_2$ ,  $\text{Co}_2(\text{OH})_3\text{Cl}$ , and  $\text{CoO}$  were investigated in the voltage range of 0.001–3 V vs.  $\text{Li/Li}^+$ . Figure 4a shows the resulting initial discharge and charge voltage profiles at a constant current density of  $1000 \text{ mA g}^{-1}$ , from which it can be seen that the  $\text{CoO}$  powders prepared at  $900^\circ\text{C}$  produce two plateaus in the first discharging process. The first of these plateaus, appearing near 0.9 V, is associated with lithium storage in  $\text{CoO}^{40-42}$ ; whereas the second plateau located near 0.6 V can be ascribed to the conversion reaction between  $\text{CoO}$  and  $\text{Li}^{40-42}$ . The slope, which is observed in the voltage range between 0.5 and 0.01 V, can be attributed to the interaction between Co particles and the electrolyte to form a solid electrolyte interface layer<sup>40-42</sup>. Conversely, the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders with small amounts of  $\text{CoCl}_2(\text{H}_2\text{O})_2$  and  $\text{CoO}$  impurities produced several plateaus in the first discharging and charging profiles. Compositionally,  $\text{Co}_2(\text{OH})_3\text{Cl}$  is a solid solution of  $\text{Co}(\text{OH})_2$  and  $\text{CoCl}_2^{43}$ ; therefore,  $\text{Co}_2(\text{OH})_3\text{Cl}$  reacts with Li according to the following reactions:  $\text{CoCl}_2 + 2 \text{Li}^+ + 2 \text{e}^- \rightleftharpoons \text{Co} + 2 \text{LiCl}$  and  $\text{Co}(\text{OH})_2 + 2 \text{Li}^+ + 2 \text{e}^- \rightleftharpoons \text{Co} + 2 \text{LiOH}^{44,45}$ . The subsequent conversion reaction of  $\text{LiOH}$  to  $\text{Li}_2\text{O}$  and  $\text{LiH}$  could be responsible for generating the additional discharge capacity<sup>46</sup>. As a result, the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders have a higher initial discharge capacity than  $\text{CoO}$  powders. Furthermore, the lithium insertion and extraction processes of  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders occur by a conversion reaction similar to that of transition metal oxides, as suggested by Tarascon *et al.* and Hu *et al.*<sup>9,46</sup> In this, crystalline Co nanoclusters and amorphous-like  $\text{LiCl}$  and  $\text{LiOH}$  could be formed by reactions of  $\text{Co}(\text{OH})_2$  and  $\text{CoCl}_2$  with Li in the first discharging process. The initial discharge capacities of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  and  $\text{CoO}$  powders were found to be 1570 and  $1142 \text{ mA h g}^{-1}$ , respectively; while their initial Coulombic efficiencies were 72 and 70%. Conversely, those  $\text{CoCl}_2(\text{H}_2\text{O})_2$  powders prepared at a low temperature of  $500^\circ\text{C}$  had initial discharge and charge capacities of 1146 and  $588 \text{ mA h g}^{-1}$ ; while their corresponding Coulombic efficiency was 51%. Figure 4b shows the cyclic voltammograms (CVs) of  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders for the first 5 cycles, in which the change in the discharging processes clearly alters the cathodic peak positions during cycling. The main cathodic peaks for the first and second discharging processes were observed at 0.9 and 1.7 V, but were subsequently moved to the lower-voltage regions during subsequent cycles. The remarkable differences in potential between the first and subsequent discharge curves were also observed, as shown in Figure S2. These results indicate that the original structure of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  cannot be reversibly recovered after the first discharge process.

Figure 4c shows the cycling performances of the powders prepared at various temperatures at a constant current density of  $1000 \text{ mA g}^{-1}$ . The discharge capacities of those powders prepared at  $700^\circ\text{C}$ , and having a primary crystal structure of  $\text{Co}_2(\text{OH})_3\text{Cl}$ , decreased from 1570 to  $872 \text{ mA h g}^{-1}$  for the first 8 cycles; but then slightly increased to  $955 \text{ mA h g}^{-1}$  during the subsequent 93 cycles. This initial decrease in the discharge capacities (2–7 cycles) was related to the transformation of the crystalline structure to a stable amorphous-like structure during cycling<sup>47,48</sup>. On the other hand, the discharge capacities of those powders prepared at  $900^\circ\text{C}$ , with a primary crystal structure of  $\text{CoO}$ , decreased steadily from 1142 to  $632 \text{ mA h g}^{-1}$  over 100 cycles. Additionally, the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders with ultrafine crystallite sizes are shown to have better cycling performance than  $\text{CoO}$  powders with a high crystallinity. The



**Figure 1** | XRD patterns of the powders prepared by spray pyrolysis at various temperatures.



**Figure 2** | Morphologies and dot-mapping images of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders prepared at  $700^\circ\text{C}$ : (a) and (b) SEM images, (c) and (d) TEM images, (e) high resolution TEM image, and (f) dot-mapping images.

$\text{CoCl}_2(\text{H}_2\text{O})_2$  powders prepared at a low temperature of  $500^\circ\text{C}$  had low discharge capacities of 1146 and  $478 \text{ mA h g}^{-1}$  for the 1<sup>st</sup> and 100<sup>th</sup> cycles, respectively. The Coulombic efficiencies of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders reached above 99% from the 7<sup>th</sup> cycle at a current density of  $1000 \text{ mA g}^{-1}$  as shown in Figure 4c. The rate performance of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders prepared at  $700^\circ\text{C}$  was demonstrated by the stepwise increase in Figure 4d from 500 to  $5000 \text{ mA g}^{-1}$  and the return to  $500 \text{ mA g}^{-1}$  in the voltage range of 0.001–3 V. For each step, 10 cycles were measured to evaluate the rate performance. The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders prepared at  $700^\circ\text{C}$  exhibited final discharge cycle capacities of 1039, 1001, 969, 936, 905, 879, 832, and  $787 \text{ mA h g}^{-1}$  at current densities of 500, 1000, 1500, 2000, 2500, 3000, 4000, and  $5000 \text{ mA g}^{-1}$ , respectively. When the current density returned to  $500 \text{ mA g}^{-1}$ , the discharge capacity recovered to  $1063 \text{ mA h g}^{-1}$  in spite of the cycling at high current densities, which indicates the good rate performance. Figure 4e shows the long-term cycling performance of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  pow-

ders prepared at  $700^\circ\text{C}$  at a high current density of  $5000 \text{ mA g}^{-1}$ , from which the discharge capacities for the 2<sup>nd</sup> and 1000<sup>th</sup> cycles were determined as 818 and  $609 \text{ mA h g}^{-1}$ , respectively. The Coulombic efficiencies of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders reached above 99% from the 15<sup>th</sup> cycle at a high current density of  $5000 \text{ mA g}^{-1}$  as shown in Figure 4e.

The Nyquist impedance plots obtained before and after the 1<sup>st</sup> and 100<sup>th</sup> cycles under a fully charged state for powders prepared at various temperatures are shown in Figure 5. In this, the medium-frequency semicircle is assigned to the charge-transfer resistance ( $R_{ct}$ ), whereas the line inclined at  $\sim 45^\circ$  to the real axis corresponds to the lithium diffusion process within the electrodes<sup>49–51</sup>. The diameter of the semicircle obtained for the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder electrode, before cycling in the medium-frequency region, was slightly smaller than those of the electrodes having primary crystal structures of CoO and  $\text{CoCl}_2(\text{H}_2\text{O})_2$  as shown in Figure 5a. Similarly, the charge-transfer resistance of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder electrode was



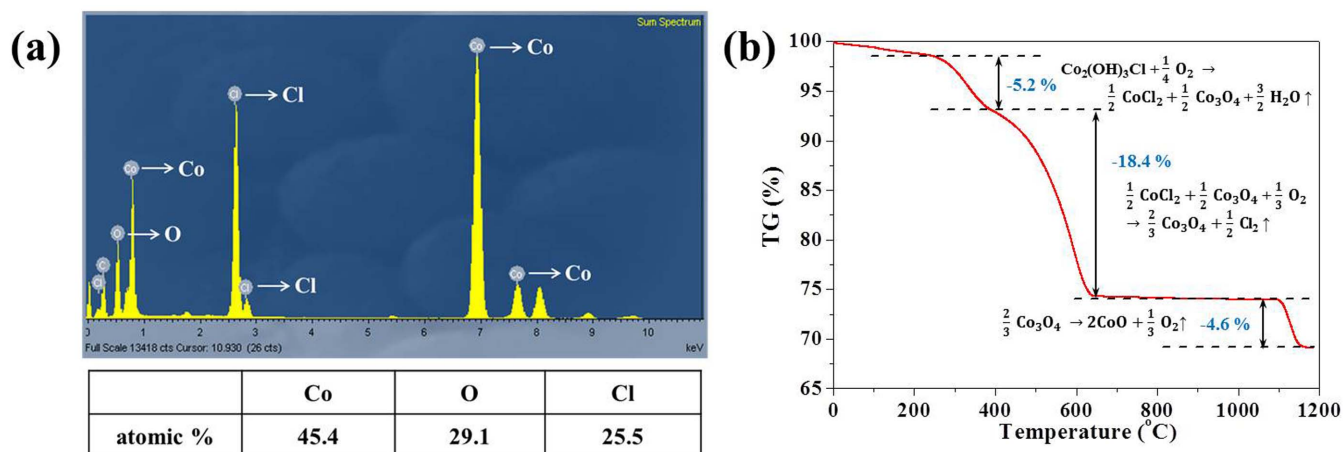


Figure 3 | (a) EDX spectrum and (b) TG curve of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders prepared at  $700^\circ\text{C}$ .

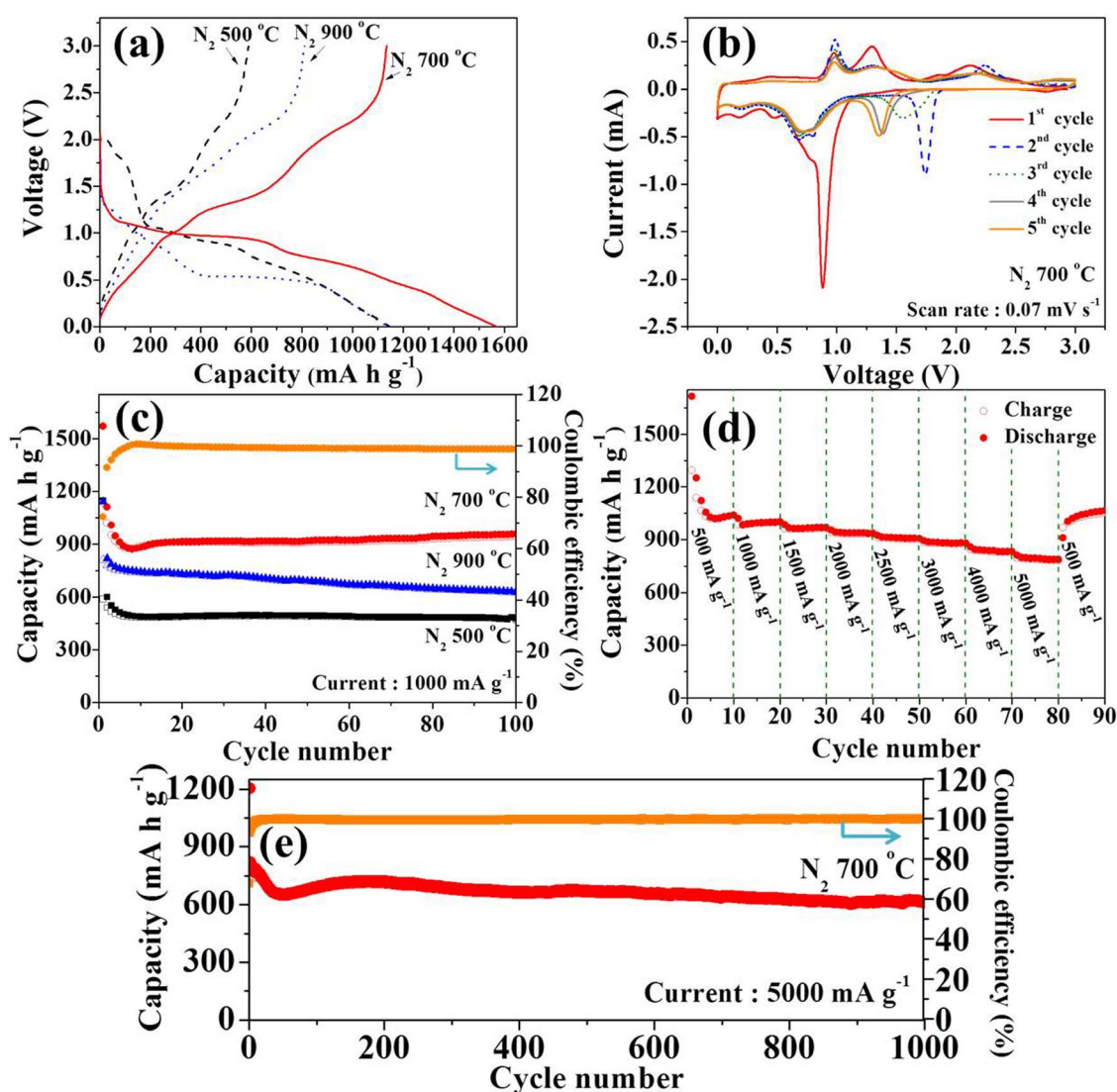
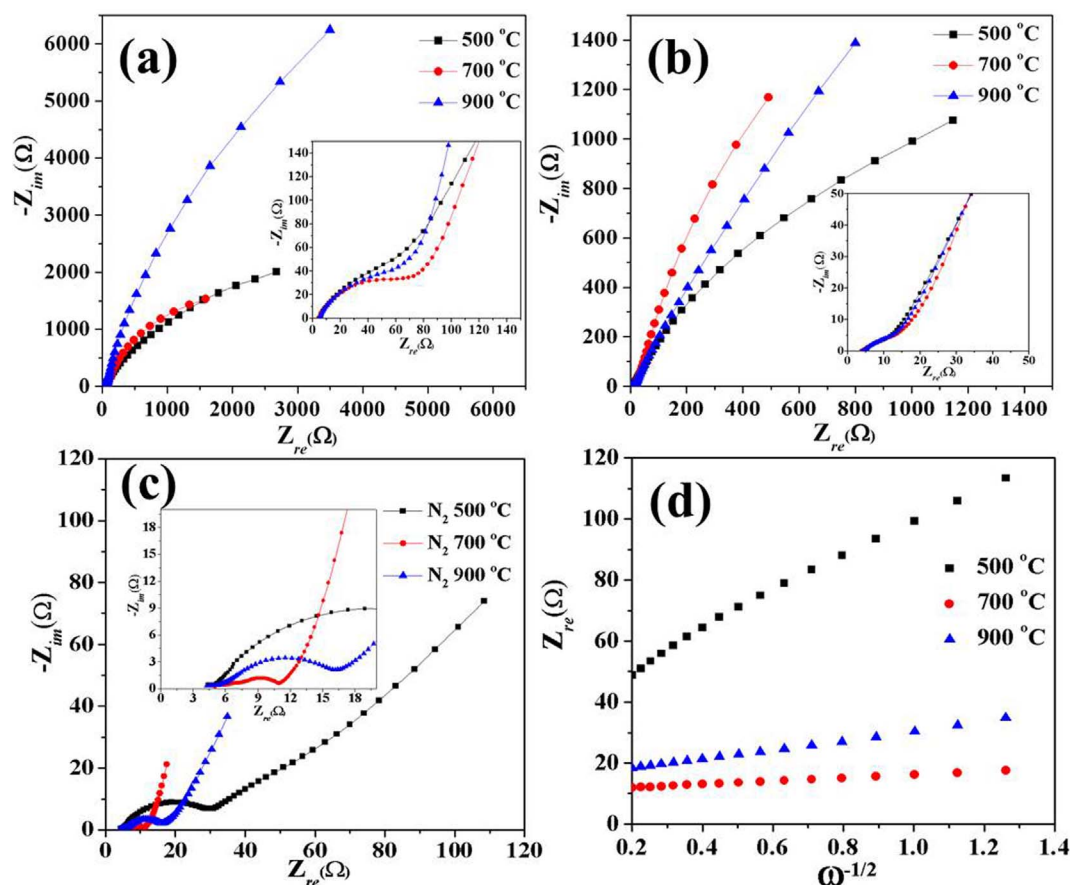


Figure 4 | Electrochemical properties of the powders prepared by spray pyrolysis at various temperatures: (a) initial discharge/charge voltage profiles at a constant current density at  $1000 \text{ mA g}^{-1}$ , (b) CVs of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders, (c) cycling performances at a constant current density of  $1000 \text{ mA g}^{-1}$ , (d) rate performance of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders, and (e) cycling performance of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders at a high current density of  $5000 \text{ mA g}^{-1}$ .



**Figure 5** | Nyquist plots of the electrochemical impedance spectra of the powders prepared at various temperatures (a) before and after the (b) 1<sup>st</sup> and (c) 100<sup>th</sup> cycles and (d) relationship between the real part of the impedance spectra ( $Z_{re}$ ) and  $\omega^{-1/2}$  after 100 cycles.

smaller than those of the CoO and  $\text{CoCl}_2(\text{H}_2\text{O})_2$  powder electrodes. The electrodes having primary crystal structures of  $\text{Co}_2(\text{OH})_3\text{Cl}$ , CoO, and  $\text{CoCl}_2(\text{H}_2\text{O})_2$  had similar charge-transfer resistances after first cycles as shown in Figure 5b. However, the diameter of the semicircle obtained for the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder electrode, after 100<sup>th</sup> cycling in the medium-frequency region, was smaller than those of the CoO and  $\text{CoCl}_2(\text{H}_2\text{O})_2$  powder electrodes as shown in Figure 5c. The structural stability of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder resulted in the low charge transfer resistance even after 100 cycles. Figure 5d shows the relationship between the real part of the impedance spectra ( $Z_{re}$ ) and  $\omega^{-1/2}$  (where  $\omega$  is the angular frequency in the low frequency region,  $\omega = 2\pi f$ ) in the low-frequency region after 100 cycles. The lower slope ( $\sigma$ , Warburg impedance coefficient) of the real part of the impedance spectra ( $Z_{re}$ ) versus  $\omega^{-1/2}$  for the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder electrode reveals a higher lithium-ion diffusion rate than CoO and  $\text{CoCl}_2(\text{H}_2\text{O})_2$  powder electrodes<sup>52–54</sup>. Figure 6 shows the morphologies of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders obtained after 100<sup>th</sup> charging process. The TEM image as shown in Figure 6a shows that the spherical morphology of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powder was maintained even after repeated charging and discharging processes. However, the powders had amorphous-like structure after cycling. The high resolution TEM image as shown inset image in Figure 6c shows the lattice fringes with a separation of 0.29 nm, which corresponds to the (300) lattice plane of  $\alpha$ -Co(OH)<sub>2</sub>. The structural stability and high lithium ion diffusion rate of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders resulted in superior electrochemical properties even at high current density.

## Discussion

The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders demonstrated good cycling and rate performances even without carbonaceous additives, which are usually

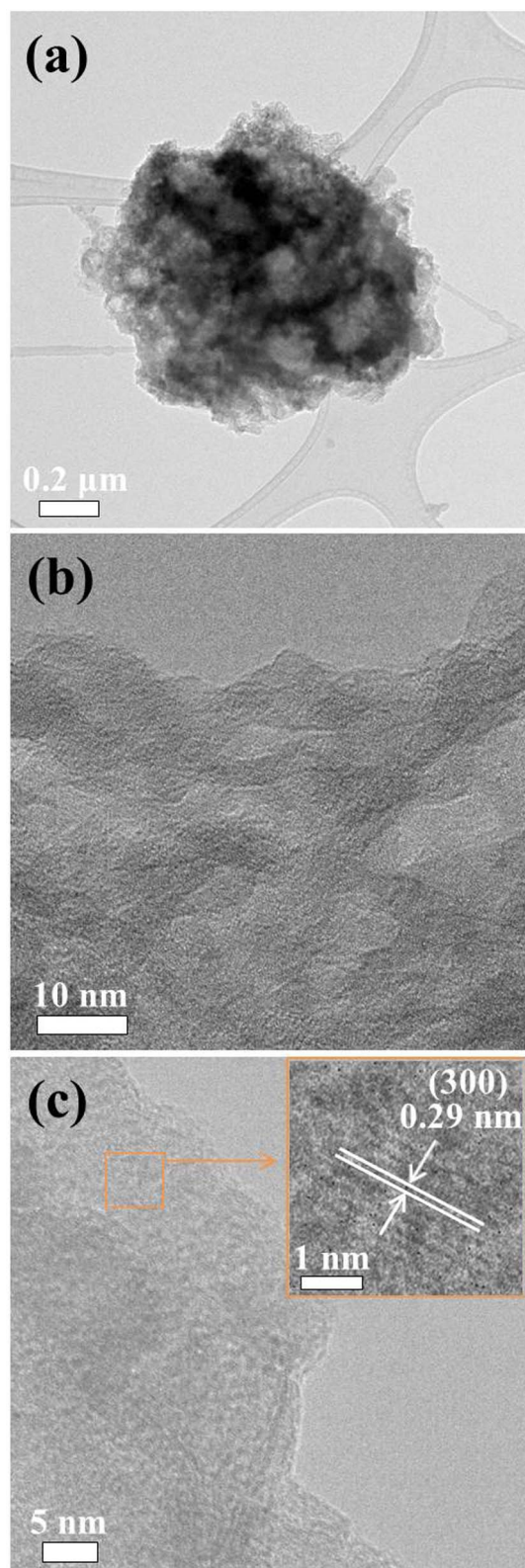
applied to improve the electrochemical properties of transition metal oxides. The pristine Co(OH)<sub>2</sub> powders prepared by the hydrothermal process had discharge capacities at a low current density of 200 mA g<sup>-1</sup> of 1599 and 910 mA h g<sup>-1</sup> for the 1<sup>st</sup> and 30<sup>th</sup> cycles, respectively<sup>44</sup>. Meanwhile, the pure CoCl<sub>2</sub> powders had respective discharge capacities of 850 and 400 mA h g<sup>-1</sup> for the 1<sup>st</sup> and 50<sup>th</sup> cycles, at a low current density of 0.2 C<sup>45</sup>. The  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders introduced in this study therefore present a more promising anode material for LIBs than either CoCl<sub>2</sub> or Co(OH)<sub>2</sub>.

The characteristics of cobalt hydroxychloride [ $\text{Co}_2(\text{OH})_3\text{Cl}$ ] prepared by a one-pot spray pyrolysis were investigated with a view to their potential application as an anode material for LIBs. Spray pyrolysis proved to be efficient for the direct preparation of  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders from a spray solution containing cobalt chloride under a nitrogen atmosphere. Moreover,  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders, which are a solid solution of Co(OH)<sub>2</sub> and CoCl<sub>2</sub>, were found to have superior electrochemical properties than more well-known anode materials such as CoO, as well as individual CoCl<sub>2</sub> and Co(OH)<sub>2</sub> materials. It was also found that the electrochemical properties of  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders can be improved by optimizing the phase purity and crystallinity, as well as developing novel nanostructures. Therefore, although this is the first such study of  $\text{Co}_2(\text{OH})_3\text{Cl}$  materials, they nonetheless show great promise as a potential anode material for LIBs.

## Methods

**Material fabrication.** The  $\text{Co}_2(\text{OH})_3\text{Cl}$ ,  $\text{CoCl}_2(\text{H}_2\text{O})_2$ , and CoO powders were prepared by one-pot spray pyrolysis from the spray solution of cobalt chloride by changing the preparation temperatures from 500 to 900 °C under nitrogen atmosphere. The concentration of cobalt chloride was 0.15 M. The spray pyrolysis system consisted of a droplet generator, a high-temperature tubular quartz reactor,





**Figure 6 | Morphologies of the  $\text{Co}_2(\text{OH})_3\text{Cl}$  powders obtained after 100<sup>th</sup> charging process.**

and a Teflon bag filter (powder collector). A 1.7-MHz ultrasonic spray generator having six vibrators was used to generate a large number of droplets, which were then carried to the quartz reactor by a carrier gas. The length and diameter of the quartz reactor were 1200 and 50 mm, respectively.

**Characterization.** The morphologies of the samples were investigated by scanning electron microscopy (SEM, JEOL JSM-6060) and transmission electron microscopy

(FE-TEM, JEM-2100F). The crystal structures of the samples were investigated by X-ray diffractometry (XRD, X'Pert PRO MPD) using  $\text{Cu K}\alpha$  radiation ( $\lambda = 1.5418 \text{ \AA}$ ) at the Korea Basic Science Institute (Daegu). Thermal gravimetric analysis (TGA, SDT Q600) was performed in air to determine the amount of carbon in the powders. The surface areas of the samples were measured by the Brunauer-Emmett-Teller (BET) method using  $\text{N}_2$  as the adsorbate gas.

**Electrochemical measurements.** The electrochemical properties of the prepared powders were analyzed in a 2032-type coin cell. The anode was prepared from a mixture of the active material, carbon black, and sodium carboxymethyl cellulose (CMC) in a weight ratio of 7 : 2 : 1. Li metal and a microporous polypropylene film were used as the counter electrode and the separator, respectively. The electrolyte was 1 M  $\text{LiPF}_6$  dissolved in a mixture of ethylene carbonate/dimethyl carbonate (EC/DMC; 1 : 1 v/v) with 2% vinylene carbonate. The discharge/charge characteristics of the samples were investigated through cycling in the 0.001–3 V potential range at various current densities. Cyclic voltammograms were measured at a scan rate of  $0.07 \text{ mV s}^{-1}$ .

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## Author contributions

G.D.P. and Y.C.K. devised the concept, designed the experiment, and wrote the manuscript. G.D.P. and Y.N.K. performed the experiments and analyzed the data. Y.C.K. supervised the project. All authors discussed the results and contributed in this manuscript.

## Additional information

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